PATENT SPECIFICATION

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(54) A PROCESS FOR THE PREPARATION OF POWDERED MALTITOL

(71) We, KOWA COMPANY LTD, a Corporation organized and existing under the laws of Japan of 6-29 Nishiki 3-chome, Naka-ku, Nagoya, Japan, do hereby declare the invention for which we pray that a patent may be granted to us and the method by which it is to be performed to be particularly described in and by the following statement:—

This invention relates to a process for the preparation of powdered maltitol. Maltitol 14-(\$\alpha\$-D-glucopyranosyl) D-sorbitol] is a disaccharide alcohol which has a sweetness of 85 to 95% of sucrose, and is recommended as sweetening agent for diabetic food (see, for example, British Patent Specification No. 1,250,952) in a similar manner to sorbitol or levulose. It is, however, recognized as being non-decomposable in intestinal tracts and also as being non-utilizable in vivo, and is, therefore, different from the other sweetening agents. Therefore, it may be also recommended as a sweetening agent in low-calorie diets.

Mahitol is also different from the other sweetening agents such as sorbitol, levulose, dextrose and sucrose, in that it is amorphous and very hygroscopic in the solid state, and it is difficult to obtain free flowing powder from the aqueous solution by conventional drying processes. Even if it is dried completely, the mass obtained changes to jelly or to a liquid state in a short space of time. For this reason, the maltitol is commercially available in about 75% aqueous solution. However, in such form, it is inconvenient to use compared with the above other sweetening agents.

According to the present invention, there is provided a process for the preparation of powdered maleirol which comprises adding a paste material as hereinafter defined suitable as food-additive to an aqueous solu-

tion of multitol, and then drying and, where necessary pulverizing, the product thus obtained to form a powder.

The paste materials of this invention are those which when mixed with water form a cohesive mixture.

The paste materials used in the present invention may be one or more of sodium alginate, propylene glycol alginate, sodium carboxymethylcellulose, sodium carboxymethylstarch, sodium starch phosphate, methylcellulose, hydroxyethyl starch, polyvinyl pyrrolidone, and polysaccharide of tamarind seed (Griloid; Trade name of Dainippon Pharmaceutical Co. Ltd. in Japan), which may be used independently or in combination. It is preferable to add 1.0 to 10.0 weight % or more of the paste materials based on the anhydrous maltitol. The upper limit of this addition is not particularly limited, but a maximum of about 10% of addition is preferable due to the decrease of the sweetness of the product.

The concentration of the maltitol in aqueous solution is not particularly limited, but it is preferable to adjust to 25 to 75% to prevent the loss of yield in the drying process

The drying process may be carried out by conventional drying method such as, for example, spray drying or vacuum drying.

In one aspect of the invention, some advantage is noted in the drying process per se, that is for example, when malittol only is dried by spray drying, it cannot be powdered because of the adhesion of the atomized malittol in jelly state on the inner wall of the chamber, and when dried in vacuum, even if the dried mass obtained is pulverized, the powder changes to a gelatinous state in a very short time.

However, according to the method of the present invention by adding the paste materials to the maltitol, it simply forms a

. id. where

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power in the spray drying, and after vacuum drying the pulverization of the dried mass is

The powdered maltitol thus obtained has a great deal of fluidity, does not change to jelly state during long storage, may be utilized in a similar manner to the common sweetening agents, and is easily soluble in water.

The effect of the addition of the paste 10

materials to the maltitol, which is illustrated by the "repose angle" which is the indication of the fluidity, can be shown from the following table. The "repose angle" is measured by gently pouring an amount of the product onto a horizontal surface to the product onto a horizontal surface to form a cone-shaped pile, and measuring the angle between the said surface and a side of the cone.

Paste Materials	Concent- ration	Repose Angle of Spray Dried Sam	of Sample	Repose Angle	of
ਦ	of paste material Note 2		After Storage for 24 hrg. at 20% R.H. at 25 G.	Just after Preparation	After Storage 24 hrs. at 20% R.H. at 25°C.
No addition		impossible to measure Note 1	impossible to measure Note 1	45	impossible to measure Note 1
Sodium alginate	1.0	. 41	42	39	41
E	2.0	39	04	0†	07
E	5.0	39	39	38	0#
Propylene glycol alginate	0.	35	38	40	41
Ξ	2.0	32	35	41	41
=	5.0	31	35	0#	40
Propylene glycol alginate + Sodium alginate	0.8	33	37	39	04
Sodium Carboxy- methylcellulose	1.0	04	41	. 38	. 39
Ξ	2.0	. 41	41	40	75
=	5.0	41	41	40	42

Paste Materials	Concentration	Repose Angle of Spray Dried Sample	of Sample	Repose Angle Vacuum Dried	of Sample
	material Note 2	Just after Preparation	After Storage for 24 brs. at 20% R.H. at 2500.	Just after Preparation	
Sodium Carboxy- methylatarch	1.0	42	43	42	77
Ξ	2.0	39	41	35	, 6 , 6
£	5.0	39	. 04	34.	. 86
Sodium starch phosphate	1.0	39	45		2 3
z	2.0	38	04	36	, t
2	5.0	38	04	30) (C
Wethylcelluloso	1.0	39	41	38	77
ε	2.0	39	40	36	o 6
2	5.0	39	39	36	C K
Hydroxyethyl starch	2.0	. 04	41	, r	2 3
Polyvinyl- pyrrolidone	2.0	40	41	, e	y (
Polysaccharide of tamarind seed (Griloid $(\overline{\mathbb{R}})$)	2.0	38	39	37	2 8 8 8
				-	

_	5		1,3	724	5
	Note 1:	Impossible to manage			
	14000 1.	, , , , , , , , , , , , , , , , , , , ,	ue to the	Example 3.	
		fact that the maltitol is in jelly state or change	ootained	Sodium alginate (45 g.) and 30 g. of	
		jelly state in measuring.	s to the	propylene glycol alginate are added to 7.5	
5	Note 2:	Added amount of th	a posta	Kg. of 50", aqueous solution of maltitol and	60
		materials are w/w % b	e paste	are dissolved with stirring, and the solution	
		the anhydrous maltitol.	ased on	is dried with a spray dryer under the same	
	Note 3:	The respective values	256 20	conditions as those of Example 1 so as to	
		average of ten experimen	aic aii	obtain multitol powder.	
10		the same conditions.	its under	Evamela 4	
	Note 4:	R.H. means relative hur	nidity	Example 4.	65
		The state of the s	naity.	Sodium carboxymethyl starch (125 g.) is added to 10 Kg. of 25% aqueous solution of	
	As is	evident from the above	results	maltitol, and is dissolved, and the solution is	•
	when the	paste materials are not a	idded to	dried with a spray dryer under the same	• •
	the maltit	ol, free flowing powdered	maltitol	condition as those in the Example 1 so as	
15	is not obt	ained by spray drying, and	l even if.	to obtain maltitol powder.	70
	in the cas	se of vacuum drying, the	product	powder.	.70
	obtained	as a powder is stored i	n a low	Example 5.	
	humidity,	such as 20% relative hum	iidity (at	Hydroxyethyl starch (100 g.) is added to	
	25° C.), it	changes to a jelly state in	ı a short	10 Kg. of 50°, of aqueous solution of	
20	time.			maltitol, and is dissolved and the solution	
	On the	other hand, the powdered	maltitol	is dried in vacuum under the same con-	75
	optained	by the method of the pre	sent in-	ditions as those in the Example 2, and then	. 73
	vention b	adding the paste materi	als loses	the obtained mass is crushed so as to obtain	
25	stored so	ne of its fluidity when s	imilarly	the multitol powder.	
23	nuste mu	that the effect of addition	n of the	With many and the second	
	As a co	erials is remarkable.	- C .	WHAT WE CLAIM IS:-	
	mercially	nparison the repose angle	or com-	1. A process for the preparation of	80
	and instan	available instant coffee t cocoa powder are 38° to	powder	powdered maltitol which comprises adding	
30	and 38° to	43°, respectively.) 42°C,	a paste material as herein defined, suitable	
	Followi	ng is a description by wa	vofev	as a food additive, to an aqueous solution of	
	ample onl	y of methods of carrying	the in-	maltitol, and then drying and, where	
	vention in	to effect.	the m-	necessary pulverizing, the product thus obtained to form a powder.	85
				2. A process as claimed in Claim 1,	
		Example 1.		wherein the amount of the paste materials is	
35	Sodium	alginate (75 g.) is added to	7.5 Kg.	1.0 to 10.0 weight % based on the	
	orbu≒ aq	ueous solution of maititol	, and is	anhydrous manito! in the solution.	00
	dissolved v	with stirring, and then the s	olution	3. A process as set forth in Claim 1 or	90
	is aried wi	th a spray dryer to obtain	3.7 Kg.	Claim 2, wherein the concentration of	
40	of arisa p	owder of maltitol. In this	step, a	marricol in aqueous solution is 25 to 75	
40	centrifugai	atomizer is used, and the	condi-	weight .0.	
	tion of spr	ay drying is as follows:		4. A process as set forth in any one of	95
	Inlet air te	innaratura 1000	1200 €	claims 1 to 3 wherein said drying sten is ner-	
	Outlet air			formed using spray or vacuum drying	
	Supply of		75° C. nl/min.	5. A process as set forth in any one of the	
45	Blow rate		n³/min.	preceding claims wherein said paste	
			00 rpm.	material is one or more of sodium alginate.	100
		25,00	o ipiii.	propylene glycol alginate, sodium car-	
				hoxymethylcellulose, sodium car- hoxymethylstarch, sodium starch	
		Example 2.		phosphate, methyl cellulose, hydroxyethyl	
	Sodium o	arboxymethylcellulose (7		SIDECD DOLUMENT DUBLE II	105
	added to H	Kg. of 75" of aqueous so	dution	polysaccharide of tamarind seed.	105
50	of matrice (ind is dissolved, and the sa	diction	6. A process for the preparation of	
	is dr æd in	vacuum by the conver	itional	powdered maltitol substantially as describ-	
	method as	follows: hot plate temper	rature	ed in any one of the specific Examples	
	00 C 1013	nours. After the obtained		nereinbefore set forth.	110
5.5	mass is coc	led, it is crushed with su	nitable.	7. Powdered multitol whenever produced	
55	hair cliver t	jounted in which was a si	eve of -1	by the process claimed in any preguding	

claim

55 pulverizer mounted in which was a sieve of

suitable mesh to separate the powder.

by the process claimed in any preceding

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